

Observation of liquid–liquid phase separation for eye lens γ S-crystallin

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γ S-crystallin (γ S) is an important human and bovine eye lens protein involved in maintaining the transparency of the eye. By adding small amounts of polyethylene glycol (PEG) to the binary aqueous bovine γ S solutions, we have observed liquid–liquid phase separation (LLPS) at -8°C and revealed that, in the binary γ S–water system, this phase transition would occur at -28°C . We have measured both the effect of PEG concentration on the LLPS temperature and protein/PEG partitioning between the two liquid coexisting phases. We use our measurements of protein/PEG partitioning to determine the nature and the magnitude of the γ S-PEG interactions and to quantitatively assess the effectiveness of PEG as a crystallizing agent for γ S. We use our measurements of LLPS temperature as a function of protein and PEG concentration to successfully determine the location of the critical point for the binary γ S–water system. This phase transition cannot be observed in the absence of PEG because it is inaccessible due to the freezing of the system. Our findings indicate that the effective interactions between γ S molecules in the binary γ S–water system are attractive. We compare the magnitude of the attraction found for γ S with the results obtained for the other γ -crystallins for which the critical temperature is located above the freezing point of the system. This work suggests that PEG can be used to reveal the existence of LLPS for a much wider range of binary protein–water systems than known previously.

protein | cataract | polyethylene glycol | phase transition | partitioning

In protein condensation diseases the primary initial step in pathogenesis is the loss of solubility of the proteins, resulting in the formation of a condensed phase. Examples of such phases include a dense liquid phase, amorphous aggregates, or crystals that form in cataract (1, 2) or the formation of fibers that are responsible for sickle cell disease (3) and Alzheimer's disease (4). In all cases the attraction between proteins is the driving force for the onset of these pathologies. Thus, the characterization of the interactions between proteins is the first step for building strategies aimed at inhibiting such diseases (5).

Liquid–liquid phase separation (LLPS), which is induced by protein–protein attractive interactions, has been directly implicated in cataract. It has been shown that this is the mechanism for lens opacification in cold cataract and that it is also operative in galactosaemic and x-ray cataracts and in hereditary cataracts in mice (1, 6). The lens proteins primarily involved in phase separation are the γ -crystallins, a family of lens-specific monomeric proteins (1). Previous LLPS studies of binary aqueous solutions of four pure individual members of the bovine γ -crystallins have shown that these proteins fall into two groups: those that show an upper consolute point at $\approx 38^\circ\text{C}$ (γ E and γ F) and those that show an upper consolute point at $\approx 5^\circ\text{C}$ (γ B and γ D) (7, 8).

Another important member of the γ -crystallin family is γ S-crystallin (γ S). Although of approximately the same size (hydrodynamic radius ≈ 2.5 nm) and molecular mass (≈ 21 kDa), the expression of γ S is different from that of the other proteins. γ S is expressed after birth and its synthesis increases with age, whereas in bovine and human lenses the other γ -crystallins are expressed mainly prenatally and their synthesis sharply decreases

after birth. It has also been found that the phase behavior of binary aqueous solutions of pure γ S differs markedly from the other γ -crystallins. Specifically, γ S solutions do not exhibit LLPS, even at temperatures as low as -10°C . Furthermore, the presence of γ S in γ B and γ F aqueous solutions significantly lowers the phase separation temperatures of these proteins in the high concentration region. These facts suggest that the presence of γ S in the lens helps to maintain transparency (9, 10).

We have experimentally and theoretically shown that polyethylene glycol (PEG) can be used to reveal LLPS in aqueous protein solutions (11). LLPS of binary protein–water systems may not be directly observable because it is inaccessible because of either the freezing of the system or the denaturation of the protein at high temperature (11, 12). The experiments with PEG can be used to deduce the location of the phase boundaries of the binary system. Here we show that LLPS of bovine γ S aqueous solutions can be induced on adding a small amount of PEG. We have measured the phase boundaries for LLPS in the ternary γ S–PEG–water system. These results are used to successfully locate the liquid–liquid phase boundary for the binary γ S–water below the freezing point of the system. Therefore, we can determine that the interactions between γ S molecules are attractive and compare the magnitude of the attraction with the other γ -crystallins.

The LLPS properties of the ternary protein–PEG–water system are described by a coexistence surface in the phase diagram. This coexistence surface represents the LLPS temperature, T_{ph} , as a function of protein concentration, c_1 , and PEG concentration, c_2 . At a fixed temperature, the LLPS properties of the system are described by an isothermal coexistence curve, which gives the concentrations (c_1^I, c_2^I) and (c_1^{II}, c_2^{II}) of the coexisting phases, I and II. The partitioning of the components in the two coexisting phases is described by tie lines connecting the points (c_1^I, c_2^I) and (c_1^{II}, c_2^{II}) of the coexistence curve. The critical point, (c_1^c, c_2^c) , is defined as the point on the coexistence curve where the condition $(c_1^{II}, c_2^{II}) = (c_1^I, c_2^I)$ occurs. The location of this point as a function of the temperature is described by a critical line on the coexistence surface (11).

Materials and Methods

Bovine γ S, which has a molecular weight of 20,800 g/mol, was isolated from 1- to 6-week-old calf lenses, obtained by overnight express from Antech (Tyler, TX). Pure γ S was isolated and purified from these lenses by standard procedures as described (7–10). The purity of the native sample was at least 98%, based on both ion-exchange and size-exclusion HPLC. To suppress aggregation of γ S, the purified protein was stored at 4°C in acetate buffer (0.2 M, pH 5) that contained DTT (0.02 M) and sodium azide (0.02%) (10, 13). PEG with average molecular weight of 1,450 g/mol (PEG1450) was purchased from Sigma-Aldrich and used without further purification.

Protein–PEG aqueous solutions were prepared as follows. The purified γ S was dialyzed exhaustively into sodium phosphate buffer

Abbreviations: PEG, polyethylene glycol; LLPS, liquid–liquid phase separation; γ S, γ S-crystallin.

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(0.1 M, pH 7.1) that contained sodium azide (0.02%). Solutions containing dilute γ S in phosphate buffer were concentrated by ultrafiltration. When the desired protein concentration was reached, a known weight of PEG was added to the protein solution. The concentration of γ S in the samples was determined by UV absorption at 280 nm, using the extinction coefficient value of $1.85 \text{ mg}^{-1}\cdot\text{ml}\cdot\text{cm}^{-1}$ calculated from the sequence (www.expasy.ch). The concentration of PEG in the samples was calculated by using the mass of PEG and the total volume of the solution. The volumetric contribution of each component was obtained by multiplying the mass of the component by the corresponding specific volume, i.e., 0.71 ml/g (14) for the protein, 0.84 ml/g for PEG (15), and 0.992 ml/g for the buffer (11).

The LLPS temperature for a given protein-PEG aqueous solution was determined by gradually lowering the temperature of the sample until clouding was observed. The cloud point was determined by the examination of the transmitted intensity-temperature profile as described by Liu *et al.* (9).

The coexisting phases were obtained by quenching the sample at fixed temperature below the coexistence surface. If after about 24 h the two coexisting phases had not separated by gravity, centrifugation was used for the separation. The protein concentration in each phase was determined by UV absorption. To determine the PEG concentration in each of the coexisting phases, an aliquot of known weight was taken from each phase, and the PEG was separated from the protein by ultrafiltration (Amicon Microcon YM-10). The concentration of PEG in the filtrate of known volume was determined by using a standardized refractive index detector (Perkin-Elmer LC-30 RI). Thus, the concentration of PEG in each aliquot could be calculated from its measured value in the filtrate. To account for the small effects of the two buffer salts (dibasic and monobasic sodium phosphate), the refractive index measurements were performed after isocratic elution of the filtrate solution on a size exclusion HPLC column ($10 \times 300 \text{ mm}$, Superdex 75 HR 10/30 from Amersham Pharmacia). The procedure was verified with protein-PEG aqueous solutions of known composition. In all cases, the measured protein and PEG concentrations in the two coexisting phases were consistent with the protein and PEG concentrations in the original, homogeneous samples.

Results

Our protein-PEG-buffer solutions can be described essentially as ternary protein-PEG-water systems. This approximation is justified by the insignificant difference in buffer concentration measured between the two coexisting phases.

We have previously shown that it is convenient to present our results in terms of the protein (component 1) concentration c_1 , and the PEG (component 2) concentration c_{2s} inside the protein-free volume. If v is the protein specific volume and $\phi = c_1 v$ is the protein volume fraction, then c_{2s} is equal to $c_2/(1 - \phi)$. The choice of c_{2s} (instead of c_2) is convenient because of the following argument. We consider as a reference system one in which the particles of component 2 have a negligible size and do not introduce specific chemical interactions in the system. In this reference case, the different values of c_2 between the two coexisting phases are entirely determined by the exclusion of component 2 from the volume occupied by component 1. Here, the condition of chemical equilibrium is expressed by the relation $c_{2s}^I = c_{2s}^{II}$. Thus, in our systems, any observed difference in c_{2s} between two coexisting phases is related to the finite size and specific chemical properties of the PEG molecules (11).

In Fig. 1, we present our experimental data (solid circles) of the coexisting values (c_1^I, c_{2s}^I) and (c_1^{II}, c_{2s}^{II}) for the γ S-PEG1450-water solutions at 265.1 K. The pairs of points representing the coexisting phases are connected by straight lines (tie lines). The dashed curve is an eye guide representing the coexistence curve. The coexisting phases were obtained by quenching samples with

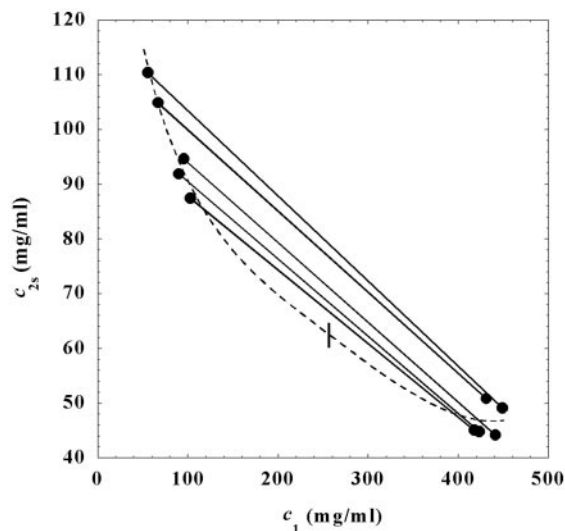


Fig. 1. Coexisting surfaces at constant temperature for the ternary γ S-PEG1450-water system. The pairs of points representing the coexisting phases (circles) are connected by the tie lines (solid lines). The dashed curve is a guide for the eye and the vertical bar locates the critical point at $c_1^c = 260 \text{ mg/ml}$. The normalized slope of the tie lines at the critical point is $(\partial c_{2s}/\partial c_1)_{T_{ph}}^c/c_{2s}^c = (-2.1 \pm 0.1)10^{-3} \text{ mg}^{-1}\cdot\text{ml}$.

the same initial protein concentration of $\approx 300 \text{ mg/ml}$ but with different initial PEG concentrations. Because the protein critical concentration, c_1^c , is equal to the average concentration $(c_1^I + c_1^{II})/2$ in the limit of $c_1^I - c_1^{II} = 0$, we determined c_1^c by plotting $(c_1^I + c_1^{II})/2$ as a function of $c_1^I - c_1^{II}$. The resulting value of the critical concentration (vertical bar in Fig. 1) is $260 \pm 10 \text{ mg/ml}$, which corresponds to a critical protein volume fraction: $\phi_c = 0.18 \pm 0.01$. To quantify PEG partitioning, we consider the normalized slope of the tie lines at the critical point $(\partial c_{2s}/\partial c_1)_{T_{ph}}^c/c_{2s}^c$. This quantity was obtained by plotting the incremental ratio $(\ln c_{2s}^I - \ln c_{2s}^{II})/(c_1^I - c_1^{II})$ as a function of $c_1^I - c_1^{II}$ and considering the limit of $c_1^I - c_1^{II} = 0$. We found $(\partial c_{2s}/\partial c_1)_{T_{ph}}^c/c_{2s}^c = (-2.1 \pm 0.1) 10^{-3} \text{ mg}^{-1}\cdot\text{ml}$.

In Fig. 2, we present our measurements of the LLPS temper-

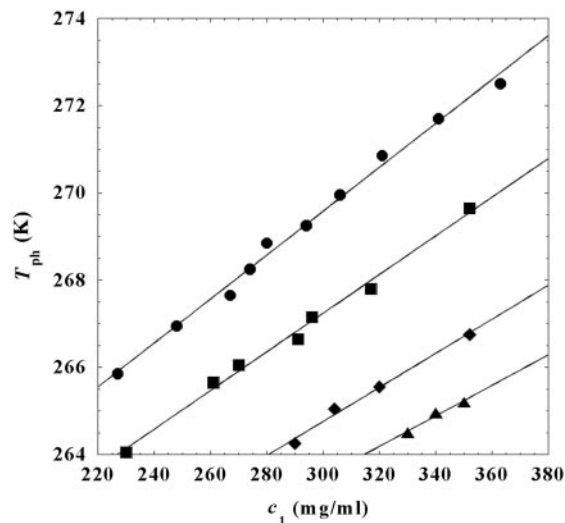


Fig. 2. LLPS temperature, T_{ph} , at constant PEG1450 concentration of $c_{2s} = 74 \text{ mg/ml}$ (circles), $c_2 = 66 \text{ mg/ml}$ (squares), $c_{2s} = 60 \text{ mg/ml}$ (diamonds), and $c_{2s} = 53 \text{ mg/ml}$ (triangles). The solid lines are linear fits to the experimental data. The protein critical concentration is $c_1^c = 260 \text{ mg/ml}$.

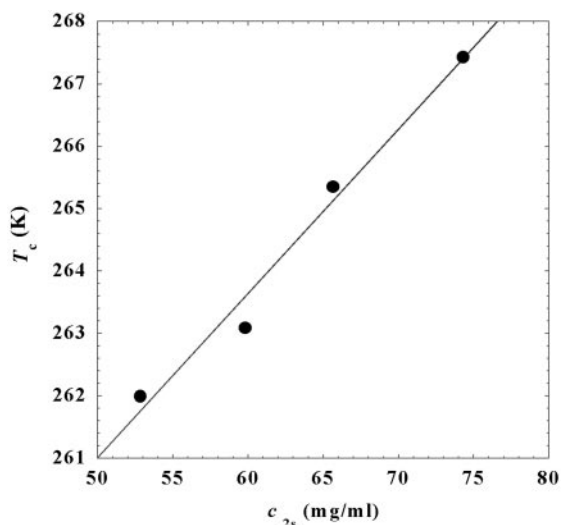


Fig. 3. Critical temperature, T_c , for the ternary γ S-PEG1450–water system as a function of c_{2s} . The dashed line is a linear fit to the experimental data with slope $(\partial T_{ph}/\partial c_{2s})_{c_1} = (0.27 \pm 0.03) \text{ K}\cdot\text{mg}^{-1}\cdot\text{ml}$.

ature, T_{ph} , for the ternary γ S-PEG1450–water solutions at constant PEG concentration of $c_{2s} = 74 \text{ mg/ml}$ (circles), $c_{2s} = 66 \text{ mg/ml}$ (squares), $c_{2s} = 60 \text{ mg/ml}$ (diamonds), and $c_{2s} = 53 \text{ mg/ml}$ (triangles). In all cases, the PEG concentration is smaller than the semidilute crossover concentration $c_{2s} = 80 \text{ mg/ml}$ (16). In Fig. 2, we can see that T_{ph} linearly increases as c_1 increases. We can fit each experimental data set with the linear function $T_{ph} = T_c(c_{2s}) + (\partial T_{ph}/\partial c_1)_{c_{2s}}^c (c_1 - c_1^c)$ (solid lines in Fig. 2). Using $c_1^c = 260 \text{ mg/ml}$ we obtained the values for both the critical temperatures, $T_c(c_{2s})$, and the slopes $(\partial T_{ph}/\partial c_1)_{c_{2s}}^c$. In Fig. 3, we plot $T_c(c_{2s})$ as a function of c_{2s} . We observe that T_c is approximately a linear function of c_{2s} with $(\partial T_{ph}/\partial c_{2s})_{c_1} = (0.27 \pm 0.03) \text{ K}\cdot\text{mg}^{-1}\cdot\text{ml}$. In Fig. 4, we plot $(\partial T_{ph}/\partial c_1)_{c_{2s}}^c$ as a function of c_{2s} . We see that $(\partial T_{ph}/\partial c_1)_{c_{2s}}^c$ increases linearly with c_{2s} and starts at zero when $c_{2s} = 0$ as it is required for a binary protein–water system (9). We found $(\partial T_{ph}/\partial c_1)_{c_{2s}}^c/c_{2s} = (0.674 \pm 0.004)10^{-3} \text{ K}\cdot\text{mg}^{-2}\cdot\text{ml}^2$.

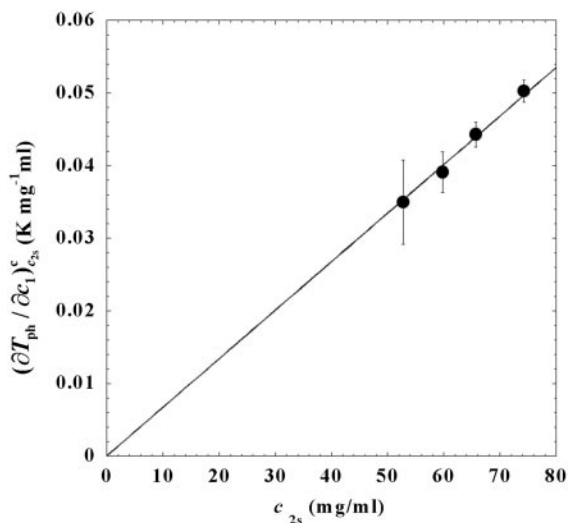


Fig. 4. Slope of the critical temperature, $(\partial T_{ph}/\partial c_1)_{c_{2s}}^c/c_{2s}$, for the ternary γ S-PEG1450–water system as a function of c_{2s} . The dashed line is a linear fit to the experimental data with slope $(\partial T_{ph}/\partial c_1)_{c_{2s}}^c/c_{2s} = (0.674 \pm 0.004)10^{-3} \text{ K}\cdot\text{mg}^{-2}\cdot\text{ml}^2$.

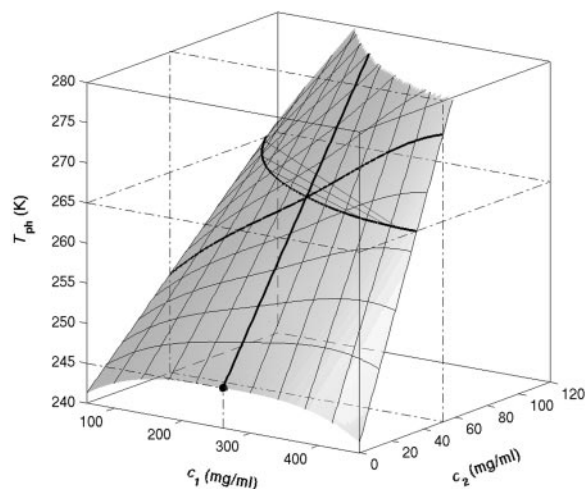


Fig. 5. Coexistence surface, $T_{ph}(c_1, c_2)$, for the ternary γ S-PEG1450–water system. Our measurements of $T_{ph}(c_1, c_2)$ reported in Fig. 2 cover the range $220 < c_1 \text{ (mg/ml)} < 360$, $40 < c_2 \text{ (mg/ml)} < 60$. A representative solid curve at constant PEG concentration is generated by the intersection of the coexistence surface and the plane at $c_2 = 53 \text{ mg/ml}$. Our concentration measurements on the coexisting phases reported in Fig. 1 are represented by the isothermal coexistence curve (solid curve) generated by the intersection of the coexistence surface with the plane at $T_{ph} = 265 \text{ K}$. The three tie lines at $T_{ph} = 265 \text{ K}$ are calculated from Eq. 4 by using $q = 0.36$. The circle at $c_2 = 0$ locates the critical point for the binary γ S–water system. The location of the critical point as a function of temperature is described by the critical line (solid curve) at $c_1 = 260 \text{ mg/ml}$.

The behavior of the coexistence surface is described by the three slopes $(\partial c_{2s}/\partial c_1)_{T_{ph}}$, $(\partial T_{ph}/\partial c_{2s})_{c_1}$, and $(\partial T_{ph}/\partial c_1)_{c_{2s}}$, which are related to each other by the mathematical relationship (9, 11):

$$\left(\frac{\partial T_{ph}}{\partial c_1}\right)_{c_{2s}} = -\left(\frac{\partial T_{ph}}{\partial c_{2s}}\right)_{c_1} \left(\frac{\partial c_{2s}}{\partial c_1}\right)_{T_{ph}}. \quad [1]$$

We apply Eq. 1 on the critical line and use the measured values of $(\partial c_{2s}/\partial c_1)_{T_{ph}}^c/c_{2s}$ and $(\partial T_{ph}/\partial c_1)_{c_{2s}}^c/c_{2s}$ to determine that $(\partial T_{ph}/\partial c_{2s})_{c_1}^c = 0.320 \pm 0.013 \text{ K}\cdot\text{mg}^{-1}\cdot\text{ml}$. This value is in satisfactory agreement with the value obtained by the direct analysis of the dependence of T_c on c_{2s} shown in Fig. 3 [i.e., $(\partial T_{ph}/\partial c_{2s})_{c_1} = (0.27 \pm 0.03) \text{ K}\cdot\text{mg}^{-1}\cdot\text{ml}$].

It is also convenient to describe the essential features of the coexistence surface within our experimental domain in terms of the variables c_1 and c_2 as shown in Fig. 5. All our data are taken in the vicinity of the point on the coexistence surface specified by the coordinates $c_1 = 260 \text{ mg/ml}$, $c_2 = 53 \text{ mg/ml}$, and $T_{ph} = 265 \text{ K}$. At this point, the values of the two principal slopes are $(\partial T_{ph}/\partial c_2)_{c_1}^c = (0.38 \pm 0.04) \text{ K}\cdot\text{mg}^{-1}\cdot\text{ml}$ and $(\partial c_2/\partial c_1)_{T_{ph}}^c/c_2^c = (-3.0 \pm 0.1)10^{-3} \text{ mg}^{-1}\cdot\text{ml}$.

We can estimate the critical temperature, T_c^0 , for the binary γ S–water system by using the relationship $T_c^0 = T_c - (\partial T_{ph}/\partial c_2)_{c_1}^c c_2$ to the critical line. This expression assumes that both the protein critical concentration, c_1^c , and the slope, $(\partial T_{ph}/\partial c_2)_{c_1}^c$, are not functions of PEG concentration. This assumption was demonstrated to be correct for the ternary γ D-PEG–water systems when PEG concentration is $\approx 50 \text{ mg/ml}$ (11). We obtain $T_c^0 \approx 245 \text{ K}$ for the binary γ S–water system. In Fig. 5, the critical point for the binary γ S–water system is located by the circle at $c_2 = 0$.

In Table 1, we report the value of the critical temperature, T_c^0 , and the critical volume fraction, ϕ_c , for the binary γ S–water system. We also report the corresponding values for the high T_c^0 γ -crystallins (γ E and γ F) and the low T_c^0 γ -crystallins (γ B and γ D) (8). All of the proteins in Table 1 have essentially the same critical volume fraction ($\phi_c \approx 0.2$), indicating that the range of

Table 1. Critical points for the bovine γ -crystallins

γ -Crystallins	ϕ_c	T_c^0 , K
γ E	0.22 ± 0.01	313
γ F	0.22 ± 0.01	309
γ B	0.19 ± 0.01	278
γ D	0.20 ± 0.01	278
γ S	0.18 ± 0.01	245

the inter-protein interactions is essentially the same for all five γ -crystallins (17). However, the difference in critical temperature of ≈ 66 K between the high T_c^0 proteins and γ S, and the difference of ≈ 33 K between the low T_c^0 proteins and γ S is the result of a corresponding difference between the magnitudes of the attraction energy. We therefore conclude that the magnitude of the attraction between γ S molecules is, respectively, $\approx 20\%$ and $\approx 10\%$ smaller than the molecular attraction found for the high T_c^0 and the low T_c^0 proteins.

Discussion

The experimentally observable feature of the coexistence surface, $(\partial c_2/\partial c_1)_{T_{ph}}^c/c_2^c$, is fully determined by the effective protein and PEG chemical potentials μ_1 and μ_2 (11). If PEG concentration is relatively small, these two chemical potentials can be expressed in the following way (11):

$$\hat{\mu}_1(c_1, c_2, T) = \hat{\mu}_1^0(c_1, T) + c_2(\partial \xi/\partial c_1)_T, \quad [2a]$$

$$\hat{\mu}_2(c_1, c_2, T) = \ln c_2 + \xi(c_1, T), \quad [2b]$$

where $\hat{\mu}_i \equiv (\mu_i - \mu_i^0)/RT$ (with $i = 1, 2$), μ_i^0 is the standard part of the chemical potential, T is the temperature, and R is the ideal gas constant. The quantity $\hat{\mu}_1^0(c_1, T) \equiv \hat{\mu}_1(c_1, 0, T)$ corresponds to the binary protein–water system and $\xi(c_1, T)$ is the first term in a series expansion describing the contribution to $\hat{\mu}_2$ over and above the ideal mixing entropy. The two cross-derivatives of the chemical potentials, $(\partial \hat{\mu}_1/\partial c_2)_{c_1, T}$ and $(\partial \hat{\mu}_2/\partial c_1)_{c_2, T}$, are both equal to $(\partial \xi/\partial c_1)_T$. This quantity characterizes the protein–PEG interactions (11).

The Slope of the Tie Lines. If we differentiate Eq. 2a with respect to c_2 at constant c_1 and T , and Eq. 2b with respect to c_1 at constant $\hat{\mu}_2$ and T , we obtain

$$\left(\frac{\partial \hat{\mu}_1}{\partial c_2}\right)_{c_1, T} = \left(\frac{\partial \xi}{\partial c_1}\right)_T = -\frac{1}{c_2} \left(\frac{\partial c_2}{\partial c_1}\right)_{\hat{\mu}_2, T}. \quad [3]$$

The normalized derivative, $(\partial c_2/\partial c_1)_{\hat{\mu}_2, T}$ coincides with the limiting value of the slope of the tie lines at the critical point and has been experimentally measured. This quantity determines the effectiveness of PEG as a crystallizing agent for γ S. Indeed, if protein crystals (the solid phase) are in thermodynamic equilibrium with the liquid phase, $\hat{\mu}_1$ must be equal to its value in the solid phase, $\hat{\mu}_1^S$. For relatively low protein concentrations, $\hat{\mu}_1^0(c_1, T) \approx \ln c_1$. Thus, using the equality of chemical potentials and Eq. 2a, we find $\ln c_1 \approx \hat{\mu}_1^S - (\partial \xi/\partial c_1)_T c_2$. This relationship gives the protein solubility, c_1 , as a function of PEG concentration, c_2 . The dependence of $\hat{\mu}_1^S$ on c_1 and c_2 is expected to be very weak. Thus the fractional decrease of protein solubility with PEG concentration is fully determined by the value of $(\partial \xi/\partial c_1)_T$, which is provided by the slope of the tie line (see Eq. 3) (11). Thus, PEG1450 reduces the solubility of γ S. We therefore believe that PEG is a useful tool not only for inducing LLPS of γ S solutions but also for favoring the formation of γ S crystals by solubility reduction.

The Excluded Volume Model of Protein–PEG Interactions. We now analyze the experimental coexisting values (ϕ^I, c_2^I) and (ϕ^{II}, c_2^{II}) to gain insight into the physical factors that are responsible for the γ S–PEG1450 interactions. We apply a simple excluded volume model that directly relates PEG partitioning to the difference in free volume fractions between the two coexisting phases. If we assume that PEG molecules can be described as ideal polymer coils and that protein molecules have a spherical shape, then due to steric hindrance, each protein will be surrounded by an adjacent region where the centers of mass of the coils are excluded, and the width, δ , of the resulting depletion layer will be proportional to the gyration radius, R_g , of the polymer coil (18–23). If α is the volume fraction available to the centers of mass of the coils, the condition of chemical equilibrium becomes $c_2^I/\alpha^I = c_2^{II}/\alpha^{II}$, where c_2/α is the polymer concentration in the free volume (21). An approximate expression for the free volume fraction, α , as a function of the hard sphere volume fraction, ϕ , is given by the well-established scaled particle theory (24–26):

$$\alpha = (1 - \phi) \exp(-A\eta - B\eta^2 - C\eta^3), \quad [4]$$

where $\eta = \phi/(1 - \phi)$, $A = 3q + 3q^2 + q^3$, $B = 9q^2/2 + 3q^3$, $C = 3q^3$, and $q = \delta/R$ is the depletion layer thickness normalized with respect to the hard sphere radius, R . The prefactor, $1 - \phi$, in Eq. 4, is the volume fraction not occupied by the spheres, whereas the exponential factor describes the effect of the depletion layers.

Because $c_2^{II}/c_2^I = \alpha(q, \phi^{II})/\alpha(q, \phi^I)$, we substitute the expression for α provided by Eq. 4 into the ratio of the free volume fractions and thereby can determine an apparent q value for each experimental tie line. We find that, within the experimental error, this quantity does not depend on the tie-line position in the coexistence curve and report the average apparent value of $\bar{q} = 0.36 \pm 0.01$. On the other hand, theoretically we expect that $q = k(R_g/R)$ where k , in the case of hard sphere-ideal chain interactions, is a known function of R_g/R (23). For PEG1450, $R_g = 1.56$ nm (14), whereas $R = 1.80$ nm is estimated from the molecular weight and specific volume of γ S. Because $R_g/R = 0.87$, the theoretical value of k is 1.03 (23) and the theoretical value of q is 0.89. Therefore, the apparent value of q is numerically ≈ 2.5 times smaller than the corresponding theoretical values. This significant discrepancy between the apparent and the theoretical q was also observed in the case of ternary γ D–PEG water systems. It appears that weak attractive interactions between PEG and γ S induce a flattening of the polymer coils near the protein surface and a corresponding reduction of the depletion layer thickness (11).

Summary and Conclusions

We have experimentally observed the liquid–liquid phase transition in ternary γ S–PEG–water ternary systems. We have used the experimental coexisting values (ϕ^I, c_2^I) and (ϕ^{II}, c_2^{II}) together with the slope, $(\partial c_2/\partial c_1)_{T_{ph}}^c/c_2^c$, to determine the γ S–PEG interactions. We have used the experimental observable feature of the coexistence surface, $(\partial T_{ph}/\partial c_2)_{c_1}$, to successfully determine the location of the upper consolute point for the binary γ S–water system. This phase transition could not previously be observed in absence of PEG because it is inaccessible due to the freezing of the system.

It is possible to argue that liquid–liquid transitions have not been observed for many binary protein–water systems because they fall outside the accessible experimental temperature range (from $\approx -10^\circ\text{C}$ to $\approx 40^\circ\text{C}$). If this is the case, PEG can be used to reveal the existence of LLPS for a much wider range of proteins than known previously.

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